# APPENDIX

#### APPENDIX C

THIS AGREEMENT, entered into this day of 1968 by and between the Commonwealth of Pennsylvania, acting through the Department of Mines and Mineral Industries, hereinafter referred to as COMMON-WEALTH and Rohm and Haas Company, Independence Mall West, Philadelphia, Pennsylvania.

#### WITNESSETH THAT:

WHEREAS the COMMONWEALTH is undertaking the construction of a treatment plant of acid mine water in the vicinity of Philipsburg, Pennsylvania and

WHEREAS the COMMONWEALTH is contemplating use of the Desal Process of Rohm and Haas Company

NOW, THEREFORE, in consideration of the premises and of the mutual covenants herein contained the parties agree as follows:

- 1. The Desal Process of Rohm and Haas shall be used in the aforesaid treatment plant.
- 2. Rohm and Haas agrees to license the Modified Desal Process to any qualified water treatment company that manufactures ion exchange equipment, and that is given the project of supplying the ion exchange equipment for the acid mine drainage plant in Philipsburg, Pennsylvania.
- 3. The plant utilizing Rohm and Haas acid mine water treating process operating on a blend of mine waters collected in the Philipsburg area having the following analysis:

pH - 2.0 to 4.5

Hardness - 600 ppm

Iron, aluminum and manganese - 35 ppm

Sulfate - 1020 ppm

Chloride - 80 ppm

(All concentrations stated in parts per million as calcium carbonate.)

will produce an effluent water having the following analysis:

pH - 7.0 to 8.5

Iron, aluminum and manganese - Less than  $0.5~\mathrm{ppm}$ 

Total dissolved solids - Less than 300 ppm

and production of such quality effluent by the Plant discharges Rohm and Haas Company from future liability.

If the Plant fails to produce water meeting the effluent standards listed above and examination of the various pieces of equipment disclose no obvious malfunction, Rohm and Haas Company will take core samples of the ion exchange resin from the ion exchange units at the Philipsburg plant and will carry out laboratory studies, using a synthetic water having the influent analysis listed above to determine whether the resin, together with other steps of the process carried out in the laboratory, will produce an effluent quality equal to or better than the effluent analysis listed above. If the effluent quality produced in the laboratory is equal to or better than that of the effluent analysis listed above, this shall be adequate evidence to establish that the resin and the Rohm and Haas process are effective in treating the Philipsburg mine waters and that the failure of the plant to produce adequate quality effluent is a result of equipment malfunction or faulty operation which is beyond the responsibility of Rohm and Haas Company.

If the laboratory studies establish that the particular resin installed in the equipment is failing to produce the required result, Rohm and Haas Company will carry out additional laboratory studies directed toward selecting an alternative resin which is effective in producing the desired result. When such a lot or lots of resin are located, it will be the responsibility of Rohm and Haas Company to furnish resin from this lot or lots to be installed in place of the resin originally installed in the Philipsburg plant.

If Rohm and Haas Company is unable to manufacture and furnish resin which, in laboratory tests, will produce effluent quality equivalent to that listed above, or to modify the conditions of the process to produce such quality effluent, Rohm and Haas Company shall be liable to a maximum of \$200,000 of the difference between the installed cost of the plant and the amount of money which can be realized by resale of the various pieces of equipment within one year of the time at which Rohm and Haas Company decided it could not furnish a satisfactory resin.

| WITNESS:  |  |  |  |  |
|---|--|--|--|--|
|   | ROHM AND HAAS COMPANY  |  |  |  |
| Secretary   |  |  |  |  |
|   | Vice President   |  |  |  |
| Governor  | COMMONWEALTH OF PENNSYLVANIA   |  |  |  |
| ВУ  | ВУ   |  |  |  |
| Budget Secretary  | Secretary of Mines and<br>Mineral Industries   |  |  |  |
| Approved as to form and manner of execution:  |  |  |  |  |
| Deputy Attorney General   |  |  |  |  |
| Company; that R.J. Whitesell, who si  | am the Secretary of Rohm and Haas<br>Igned this agreement on behalf of Rohm<br>Sident of said Rohm and Haas Company; |  |  |  |
| that said agreement was duly signed Haas Company by authority of its gov of its corporate powers. | for and in behalf of said Rohm and verning body, and is within the scope   |  |  |  |
|   |  |  |  |  |
|   | (Corporate Seal)   |  |  |  |
|   |  |  |  |  |

### Equipment List

- I Feed System
  - A. Mine Hole #1
    - (2) Pumps 500 gpm @ 180' TDH, 40 hp
  - B. Mine Hole #3
    - (2) Pumps 500 gpm @ 108' TDH, 25 hp
  - C. Red Moshannon
    - (2) Pumps 500 gpm @ 37' TDH, 10 hp
- II Ion Exchangers
  - (4) Tanks 11' diameter x 13' str. side
- III Decarbonator
  - (1) Spray Nozzle
  - (1) Tank
- IV Aerator
  - A. (1)  $6' \times 6' \times 22'$  high, wood slat aerator
  - B. (1) Blower 500 CFM @ 9", 1 hp
- V Settling Basin
  - (2) 40' diameter x 8' deep
- VI Lime Softener, Solids Contact Type
  - (1) 25' diameter x 15' high
- VII Recarbonation
  - (1) Mixing Tee
- VIII Gravity Filters
  - (3) 10' diameter x 10' high
  - IX Ground Storage Tank
    - (1) 40' diameter
  - X Regeneration Station with Ammonia Recovery
    - A. (1) Day tank, 5,000 gal
    - B. (2) Chemical Precipitators, 12' diameter, 15,000 gal conical bottom
      - (2) Turbine Agitator, 15 hp
    - C. (2) Plant and frame pressure filters with cake conveyor, 1 hp
    - D. (1) Stripper
    - E. (1) Distillate Storage

### Equipment List (continued)

- XI Chemical Feed System
  - A. Lime
    - (1) Silo 12' diameter x 30' high, cone bottom
    - (1) Gravimetric Feeder
    - (1) Slaker 1000 #/hr with grit remover
    - (1) Storage tank, 5,000 gal with turbine agitator, 3 hp
  - B. Carbon Dioxide
    - (1) Storage Vessel 12' diameter x 30' LG (liquid form)
    - (1) Evaporator
  - C. Ammonia
    - (1) Storage Vessel 12' diameter x 30' LG
  - D. Coagulant Aid
    - (1) Tank with mixer, 1/4 hp

## XII Pumps

- A. Ion Exchange Regeneration
  - 1. Ammonia Feed (1)
  - 2. Lime Transfer Pump (1), 1/3 hp
  - 3. Lime Slurry Pumps (2), 1/2 hp
  - 4. Slurry Pumps (2) 1/2 hp
- B. Lime Softener
  - 1. Recirculation
  - 2. Lime Feed (2), 150 gph, 1 hp
  - 3. Coagulant Aid Feed, (2), 3/4 hp
- C. Gravity Filter
  - 1. Backwash water to filters, 800 gpm @ 58', 20 hp
  - 2. Backwash water to softener
  - 3. Sump Pump, 100 gpm @ 25', 3/4 hp
- D. Service

### XIII Instrumentation

- A. Flow Meters
  - 1. Panel mounted indicate, record, totalize
    - a. raw water
    - b. lime softener influent
    - c. plant effluent
  - 2. Locally mounted, indicating only
    - a. ion exchange inlet (4)
    - b. gravity filter inlet (3)
    - c. lime feed system (3)
  - 3. Locally mounted indicate, record, totalize
    - a. lagoon effluent

### Equipment List (continued)

B. Specific Conductivity

Panel mounted, indicate, record

- a. raw water
- b. ion exchange effluent (4)
- c. settling basin effluent
- d. plant effluent
- C. pH
  - 1. Panel mounted, indicate, record
    - a. raw water
    - b. ion exchange effluent (4)
    - c. settling basin effluent
    - d. recarbonation effluent
    - e. plant effluent
  - 2. Panel mounted, indicate only
    - a. lime softening effluent
    - b. decarbonator effluent
- D. Total Hardness

Panel mounted, indicate, record

- a. raw water
- b. lime softener effluent
- E. Turbidity

Panel mounted, indicate, record

- a. raw water
- b. lime softener effluent
- c. plant effluent
- F. Pressure Differential

Locally mounted, indicate only

- a. inlet and outlet of ion exchangers (8)
- b. downstream from main pressure relief valve
- c. inlet and outlet of gravity filter
- G. Temperature

Locally mounted, indicate only

a. inlet to ion exchangers (4)

# AMD MATERIAL BALANCE

# Sludge Produced

# Aeration Settling Basins

| Mn(OH) <sub>2</sub>                   | 41     | #/Day |   |              |
|---------------------------------------|--------|-------|---|--------------|
| Fe(OH) <sub>3</sub>                   | 1525   | #/Day |   |              |
| A1(OH) <sub>3</sub>                   | 297    | #/Day |   |              |
| J                                     | 1863   | #/Day | - | 1,863 #/Day  |
| Lime Softener                         |        |       |   |              |
| CaCO <sub>3</sub>                     | 6258   | #/Day |   |              |
| Mg(OH) <sub>2</sub>                   | 646    | #/Day |   |              |
| Mn(OH) <sub>2</sub>                   | 112    | #/Day |   |              |
| <b>-</b>                              | 7016   | #/Day | - | 7,016 #/Day  |
| Ammonia Recovery                      |        |       |   |              |
| Ca Cl <sub>2</sub>                    | 78     | #/Day |   |              |
| CaSO <sub>4</sub> . 2H <sub>2</sub> O | 9781   | #/Day |   |              |
| Ca(OH) <sub>2</sub>                   | 422    | #/Day |   |              |
| <b>4</b>                              | 10,281 | #/Day | - | 10,281 #/Day |
|                                       |        | Total | _ | 19,160 #/Day |

